



# **MULTICRITERIA COMPARISON OF THREE TECHNOLOGIES FOR THE TREATMENT OF 42 PFAS IN DRINKING WATER USING A COMPREHENSIVE EXPERIMENTAL APPROACH**



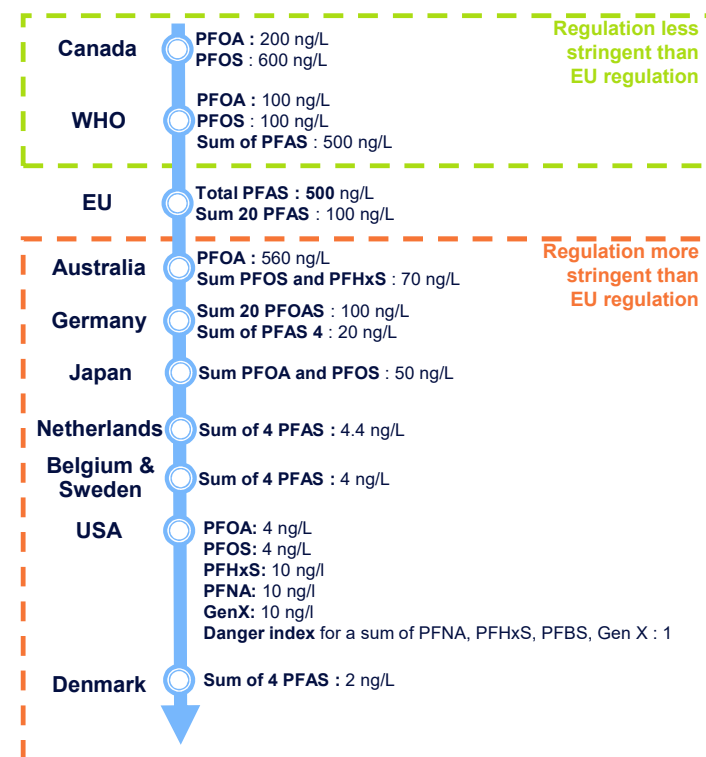
## Agenda

- 1. Context & treatment challenge for DW production**
- 2. Methods**
- 3. Relevant results on GAC, PAC, membranes & IEX for PFAS**
- 4. Multicriteria comparison of technologies: Case study**
- 5. Conclusion & perspectives**



# 1. Context

- ❑ **PFAS : Man-made chemicals (more than 14 000 compounds)** widely used **since the 1940s thanks to exceptional properties** (*stability of polarized C-F bonds*)
- ❑ **Worldwide massive contamination** by PFAS more and more quantified and mediatized  
*Ex In Europe (Le Monde, Feb 2023) : more than 17,000 sites > 10 ppt - more than 2,100 clusters > 100 ppt*  
**No clear picture of the spreading** : issue for wastewater and leachate discharge - Sludge disposal - Resources & Drinking water management
- ❑ **Priority on DW** driven by sanitary risks and drastic current and evolving regulations  
 USA : focused on **6** PFAS  
 Europe : linked to sum of **20** & total compounds



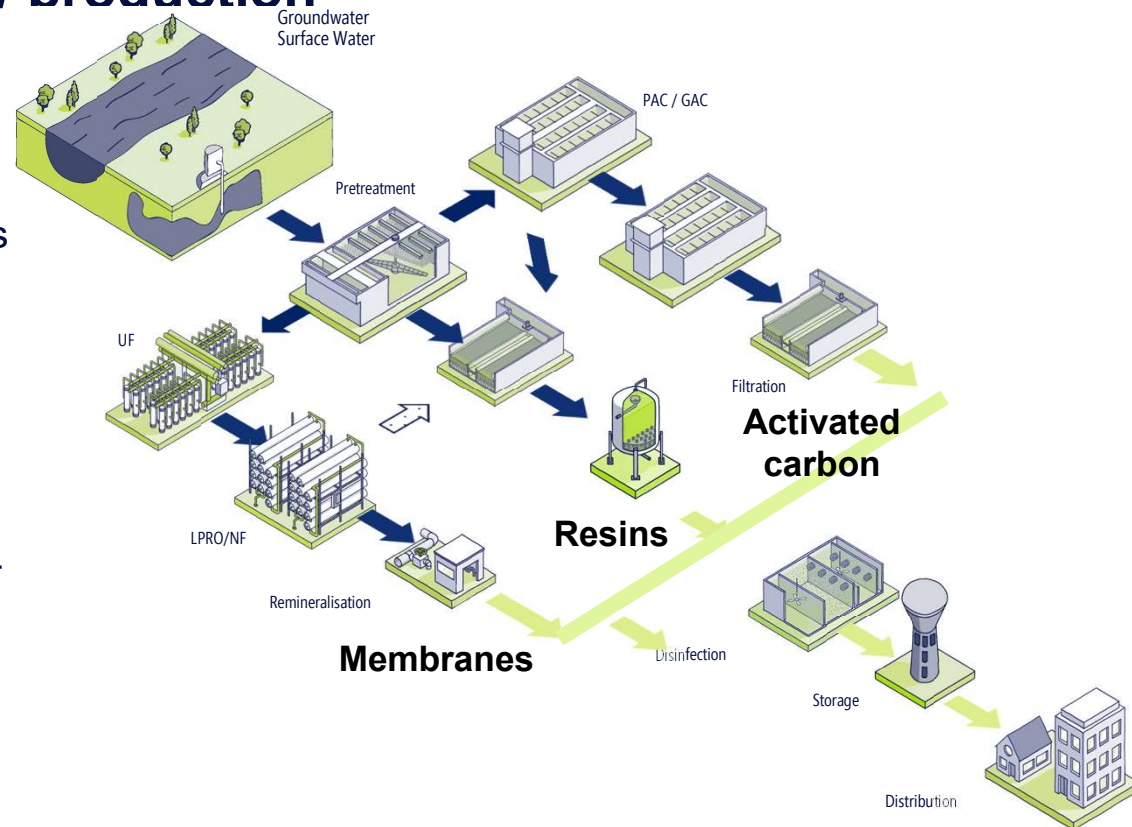
**Main concerned 6 PFAS :**  
 PFBS – PFOS – PFOA – PFHxS – PFNA – GenX

**PFAS : challenges for water professionals to qualify/quantify contamination & to adapt treatment for risks control**



# 1. Treatment challenge for DW production

- ❑ What are the treatment performances for various types of polluted resources ?
- ❑ How to combine them?
- ❑ How to integrate them in existing assets?
- ❑ How to select the best (technical + economical + environmental) solution for each specific case to comply with local regulation ?



What is the best treatment strategy for each specific case ?



## 2. Methods

# PFAS

*Regulation,  
occurrence, properties*

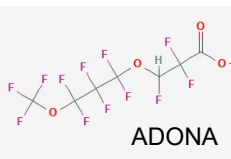
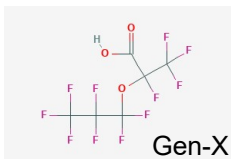
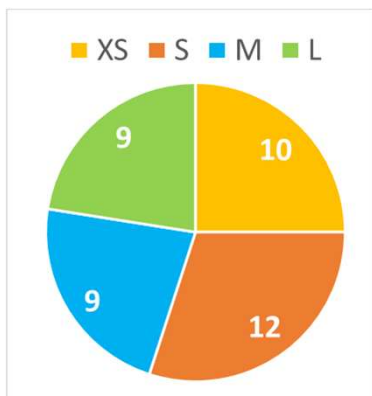
LQ

1 - 5 ng/L

*Excepted 20 ng/L  
for PFPrA*



UHPLC MS MS (WATERS)



## Activated Carbon

2 *GAC*  
3 *PAC*



# Membranes

2 LPRO  
2 NF



## IEX resins



## 2 water matrices

Clarified surface water  
(DOC  $\approx$  2 mg/L)  
Groundwater  
(DOC  $\approx$  1 mg/L)



## Step 1: Lab Scale (9 months)

### *Treatment efficiency in controlled conditions*



## Step 2: Mini pilot & Pilot scale (6 months)

## Transpose laboratory results to industrial scale



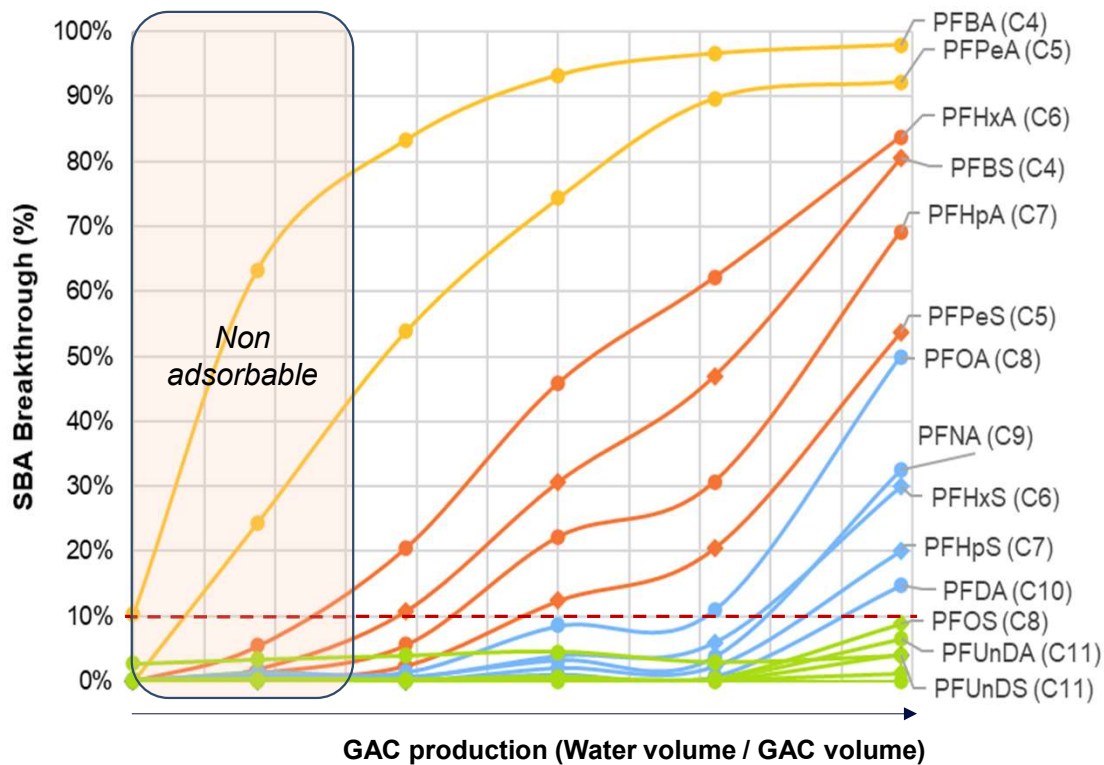
**≈ 200 samples    ≈ 20 000 analysis**



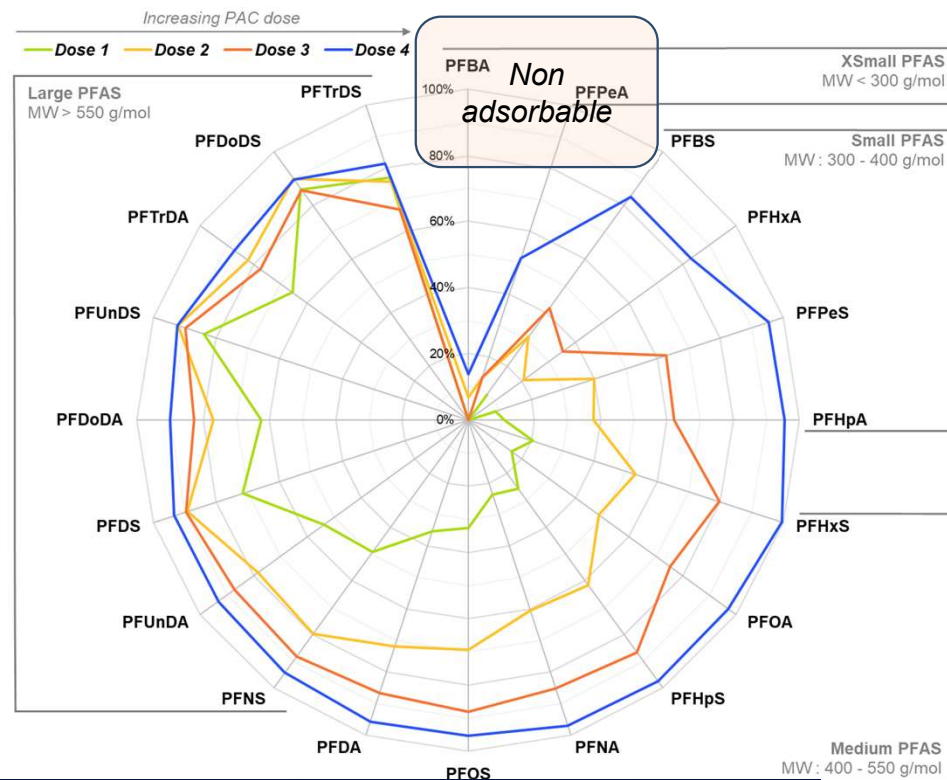
### 3. Relevant results on GAC & PAC for PFAS (20-DW)

Ex. for groundwater - DOC=1 mg/L

Ex. PFAS **GAC** breakthrough @ 10% - CT = 15'



Ex. PFAS removal @ different **PAC** doses - CT = 30'



**XS-S PFAS : very low adsorbable compounds needing high, not realistic, GAC renewal or PAC doses**



### 3. Relevant results on GAC & PAC for PFAS (20-DW)

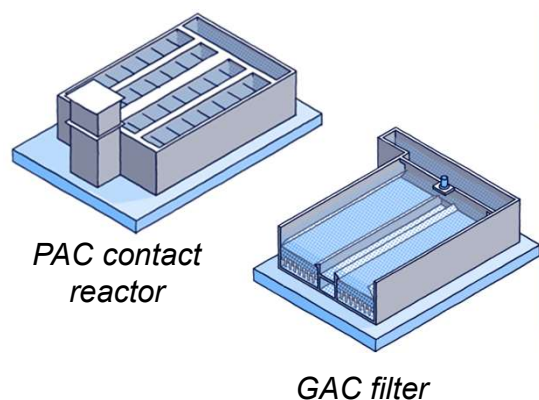
#### ❑ Adsorption efficiency

- With the PFAS MW
- Depending on functional group of PFAS: sulfonic acid (-S) > carboxylic acid (-A) - Neutral > anionic > cationic
- With the OM in the water matrix
- = No impact of pH
- With the GAC-PAC type (*agglomerated media, high surface specific, high Iodin index*)
- With increased contact time

#### ❑ Operational recommendations

Ex : Groundwater  
DOC = 1 mg/L

PFAS size	PFAS (20-DW)	20 other PFAS	% removal for PAC @ 50 ppm - CT = 30'	GAC breakthrough @ 10 % - CT = 12'
<b>XSmall PFAS</b> (MW < 300 g/mol)	PFBA, PFPeA	PFPrA, TFMS, PFEtS, PFMPA, PFMBA, 3:3 FTCA, FBSA	15 - 70 %	< 3 500 VV
<b>Small PFAS</b> (MW : 300-400)	PFHxA, PFHpA <b>PFBS</b> , PFPeS	<b>GenX</b> , ADONA, 5:3 FTCA, 4:2 FTS, 6:2 FTS FBSE, N-Me-FBSE	60 - 95 %	< 10 000 VV
<b>Medium PFAS</b> (MW : 400-550)	<b>PFOA</b> , <b>PFNA</b> → PFDA <b>PFHxS</b> → <b>PFOS</b>	FOSA, N-Me-FOSE, 9CI-PF3ONS	80 - 99 %	< 20 000 VV
<b>Large PFAS</b> (MW > 550 g/mol)	PFUnDA → PFTrDA PFNS → PFTrDS	PFTeDA PFHxDS	90 - 99 %	> 20 000 VV



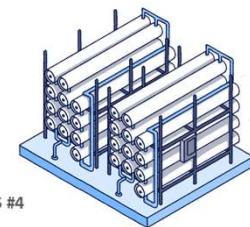
- ❑ AC can be a solution to treat PFAS pollution depending on the type of PFAS, concentration & matrix
- ❑ Challenge for S and XS PFAS : Non / low adsorbable compounds



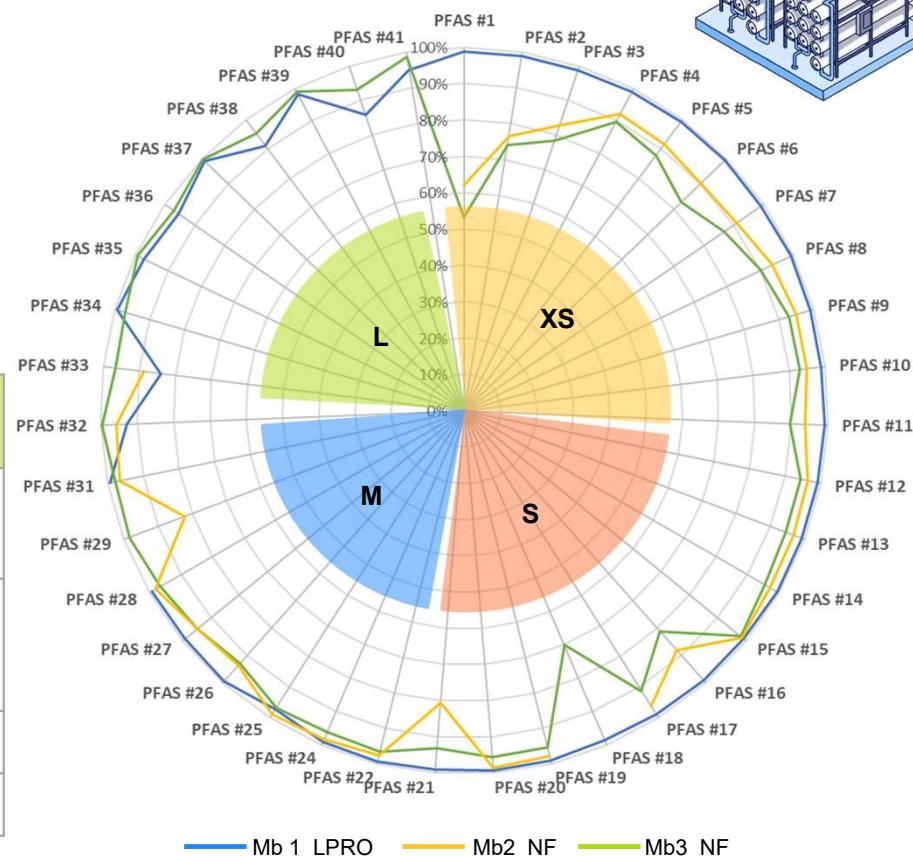
### 3. Relevant results on membranes



Trials simulating a **3-stages** plant operating at **85% recovery**



	Very small PFAS (MW<300g/mol)	Small PFAS (300-400 g/mol)	Medium PFAS (400-550 g/mol)	Large PFAS (MW > 550 g/mol)
<b>Ex from EU DW reg</b>	PFBA, PFPeA	PFHxA, PFHpA <b>PFBS</b> , PFPeS	<b>PFOA</b> <b>PFNA</b> → PFDA <b>PFHxS</b> → PFOS	PFUnDA → PFTTrDA PFNS → PFTTrDS
<b>Other</b>	PFPrA, TFMS, PFEtS, PFMPA, PFMBA, 3:3 FTCA, FBSA	<b>GenX</b> , ADONA, 5:3 FTCA, 4:2 FTS, 6:2 FTS FBSE, N-Me-FBSE	FOSA, N-Me-FOSE, 9CI-PF3ONS	PFTeDA PFHxDS
<b>NF</b>	<b>50 – 80%</b>	<b>80 – 90%</b>	<b>&gt; 90%</b>	<b>&gt; 90%</b>
<b>LPRO</b>	<b>&gt; 90%</b>	<b>&gt; 90%</b>	<b>&gt; 90%</b>	<b>&gt; 90%</b>



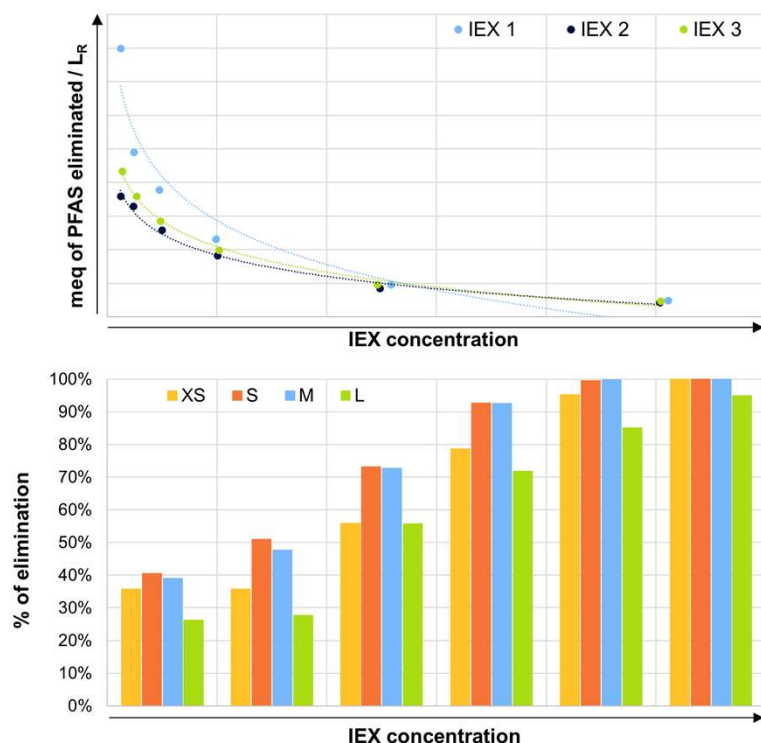
- ❑ XS & S compounds: LPRO very efficient (>90%) / nanofiltration partial rejection (50 – 90%)
- ❑ Medium & Large PFAS: LPRO and NF efficient (> 90%)



## 3 – Relevant results on Ion Exchange resins (IEX)



IEX batch test – groundwater (DOC = 1 mg/L)



### Resins efficiency

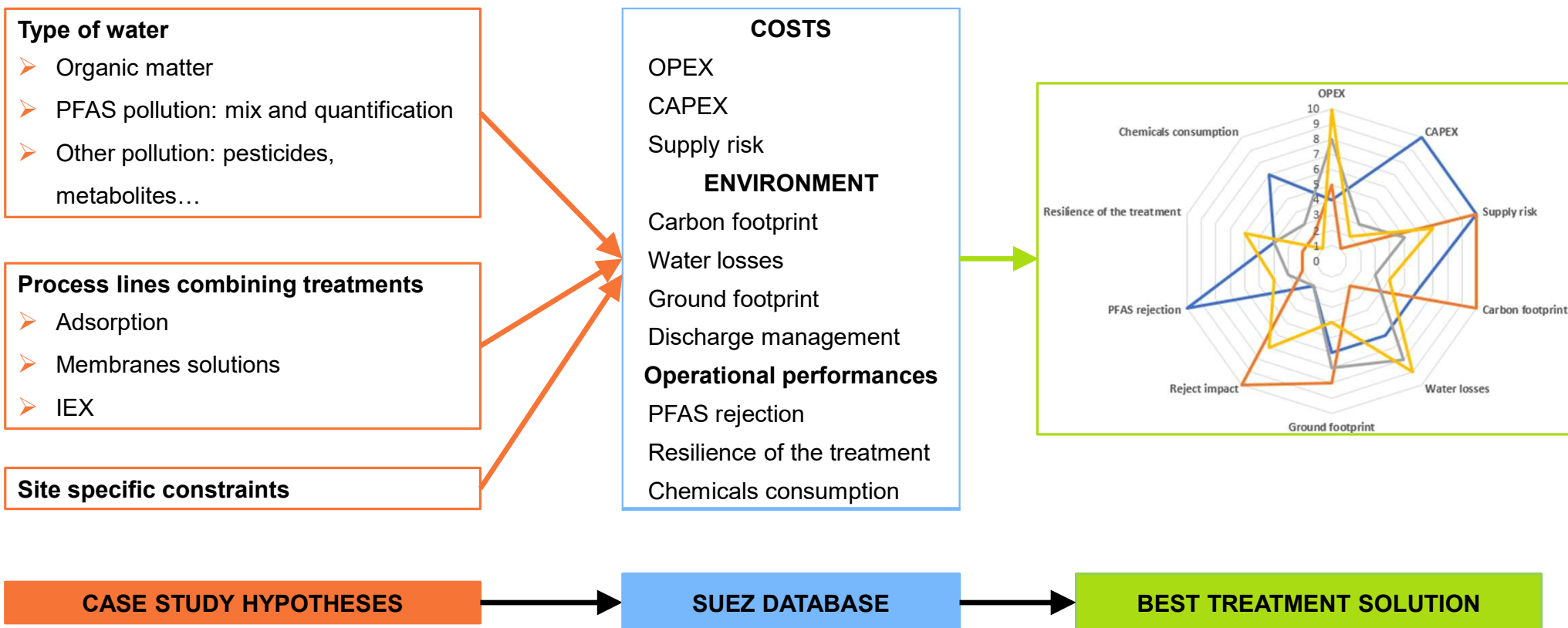
- No significant difference between the 3 tested resins
- No significant difference between XS & S compounds : advantage on Activated Carbon treatment
- No impact of NOM level (for DOC < 2 mg/L)
- Pilot test & economic and technical comparison to Activated Carbon on-going



- ❑ Resin can be a technical solution to treat PFAs pollution - Adapted to treat S and XS compounds
- ❑ Costs & environmental approach to be managed



## 4. Multicriteria comparison of technologies





## 4. Case study

### Context

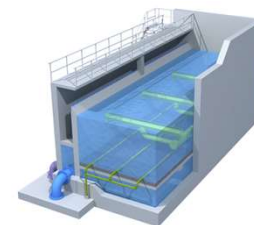
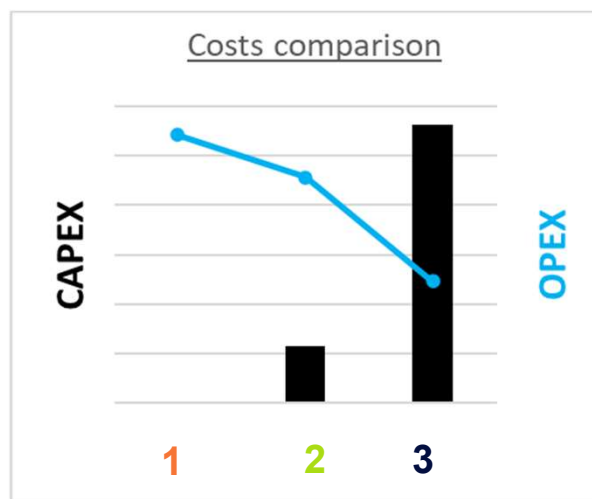
- ❑ French groundwater treatment plant (11 000 m<sup>3</sup>/d)
- ❑ Existing treatment = **GAC**
- ❑ **Industrial pollution 6:2 FTSA**  
9 PFAS detected including 6:2 FTSA degraded in by-products
  - PFHxA (C6)
  - PFBA (C4)
  - PFPeA (C5)

Inlet	Target
Σ20 PFAS 0,14 - 0,31 µg/l	Σ20 PFAS 0,1 µg/l

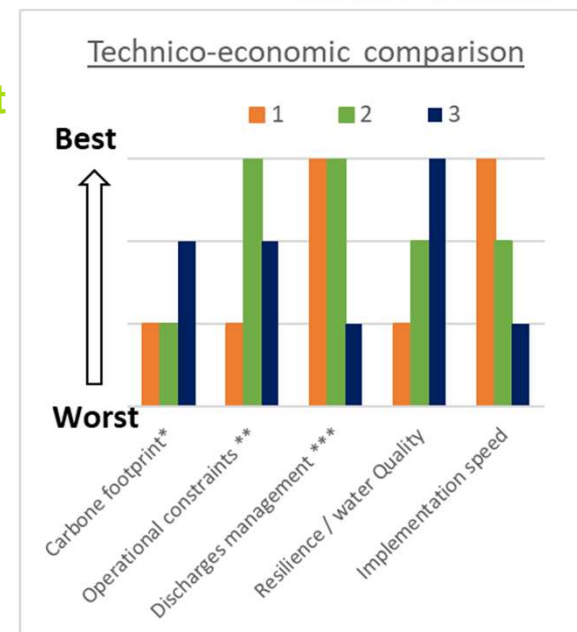
- ❑ DWTP **refurbishment** project

### Results

- ❑ 3 proposed treatment lines:
  1. **Increase GAC regeneration**
  2. **GAC with continuous replacement**
  3. **Mix GAC / LPRO**



Carbazur-Up ®



\* GAC regenerated, energy for mb only, excl CIP and antiscalant

\*\* GAC charge regeneration, chemical, membrane washing

\*\*\* quantity, pollutant loads, diversity of discharges

**Option 2 is the most adapted to the local constraints (discharges, manpower). It allows to optimize existing assets.**



## 5. Conclusion and perspectives

### Priority 1 → drinking water production

1. Refurbishment / strengthening to optimize existing assets
2. New DWTP design

→ Need of **precise knowledge** about efficiency of each process



- Large panel of PFAS
- Analytical complexity
- Complex lab and pilot trials
- Numerous impacting factors

→ Considering each **site-specific** context



### Priority 2 → Destruction

But, when removed from the water cycle, ...  
**don't put back into the resource !**

- ☐ Destruction treatments needed
- ☐ Many key players in the US, China...
- ☐ Existing solutions must be studied in terms of efficiency but also economic and environmental performance
- ☐ And demonstrations are required !



**THANK YOU FOR  
YOUR  
ATTENTION**

